

Fig. 1. IR-spectrum of polyphenol leaf from urtica dioica L.

of the visible region. The entire IR zone is a conventional electron and oscillatory transformation, in the range of 4000–12500 cm<sup>-1</sup> wavelength range, in the

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Fig. 2. IR-spectrum of isolated polyphenol is olated

range of 625–4000 cm<sup>-1</sup> in the range of molecules oscillating, in the range 50–625 cm<sup>-1</sup> with rotational fluctuations distant regions.

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## THE INFLUENCE OF ZEOFORMING PROCESS TEMPERATURE ON THE PRODUCTS COMPOSITION

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The most promised processes for the oil refining at the moment are processes that use zeolites as catalysts. The zeolites popularity as a catalyst is due to a number of factors – low cost, stability and resistance to catalytic poisons. Process for the production of high-octane gasoline components which uses zeolites as a catalyst, it is the Zeoforming. The purpose of this work is to consider how the process temperature effects on the products composition, as well as to determine the optimum temperature of the process, in terms of involving zeoformats in gasoline blending.

Sample	SGC %vol.	Zeoformat at a temperature, % vol.			
		375 °C	400°C	425 °C	
Aromatics	0.62	10.26	24.07	25.25	
Olefins	1.14	4.81	4.31	3.62	
Naphthenes	19.35	7.74	9.37	6.29	
Iso-paraffins	38.25	43.94	37.86	38.98	
N-paraffins	40.64	33.25	24.36	25.86	
Benzene	0.17	0.07	3.94	4.17	

 Table 1.
 Composition of feedstock and products

Component content 0/ wit	Gasoline brand				
Component content, % wt.	RON-92	RON-95	RON-98		
Zeoformat 375 °C	75	65	55		
Alkylate	5	10	15		
Toluene	20	25	30		

 Table 2.
 Gasoline blending recipes

## Table 3.Gasoline properties

Doromator		Dequirements [1 2]			
Parameter	RON-92	RON-95	RON-98		
RON/MON	92.5/85.2	95.6/87.8	98.7/90.5	92/83; 95/85 98/88	
SVP, kPa	95.6	85.0	74.4	35-100*	
Density at 15°C, kg/m <sup>3</sup>	726.4	735.8	745.2	725-780	
Benzene, %vol.	0.13	0.14	0.16	>1**	
Aromatics, % vol.	24.03	27.32	30.73	>35**	

\*in the winter and off-season; \*\*for 3–5 emission class

The Zeoforming process was implemented in a laboratory catalytic unit under varying temperature conditions. Stable gas condensate (SGC) was used as the process feedstock, the feedstock volume flow rate was 2 h<sup>-1</sup>, the pressure was 2.5 MPa, and the process temperature was varied between 375– 425 °C with increments of 25 °C. The composition of feedstock and products were determined by gas chromatography. The results are presented in Table 1.

From the results presented in Table 1, it follows that with increasing process temperature, the aromatic hydrocarbons content in the products increase, incidentally benzene content. This effect is explained by increase in the rate of target reactions of naphthenes dehydrogenation and paraffins dehydrocyclization. In addition, from the results present-

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ed in Table 1 it follows that the most promised for the gasoline production is a product obtained at a temperature of  $375 \,^{\circ}\text{C}$  – for this zeoformat are observed the highest content of high-octane iso-paraffins and the lowest content of benzene and aromatic hydrocarbons, the content of which in commercial gasolines is restricted [1, 2].

To confirm the obtained results, using the software "Compounding" [3] and additional blending components (alkylate, toluene), recipes for production gasoline were developed (Table 2). The gasoline properties, obtained according to the developed recipes, are presented in Table 3.

From the results presented in table 3, it follows that gasolines produced according to the developed recipes meet the requirements of the standards [1, 2].

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